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	TR	ANSMITTAL LETTER	TO THE UNITED STATES	205744US0PCT
,		DESIGNATED/ELECT	ED OFFICE (DO/EO/US)	U.S. APPLICATION NO. (IF KNOWN, SEE 37 CF)
	(CONCERNING A FILI	NG UNDER 35 U.S.C. 371	09/830149
ITER		ONAL APPLICATION NO.	INTERNATIONAL FILING DATE	PRIORITY DATE CLAIMED
		CT/EP99/07899	19 OCTOBER 1999	21 OCTOBER 1998
PPLI	CANT	C(S) FOR DO/EO/US	G A LUBRICITY EFFECT FOR MIT	NERAL OIL MIDDLE DISTILLATES
		ENDEROTH, et al.	tatas Designated/Elected Office (DO/EO/IJS) the following items and other information:
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1.	\boxtimes		items concerning a filing under 35 U.S.C. 3	
2.			QUENT submission of items concerning a f	
3.	×	This is an express request to be (6), (9) and (24) indicated below	gin national examination procedures (35 U.S.w.	S.C. 371(f)). The submission must include itens (5),
4.	Ø		e expiration of 19 months from the priority d	late (Article 31).
5.	Ø		plication as filed (35 U.S.C. 371 (c) (2))	,
٠.	_	• • • • • • • • • • • • • • • • • • • •	quired only if not communicated by the Inte	rnational Bureau).
		· ·	ted by the International Bureau.	,
			application was filed in the United States Re	eceiving Office (RO/US).
6.	\boxtimes		on of the International Application as filed (3	
		a. \(\square\) is attached hereto.		
		b. has been previously s	submitted under 35 U.S.C. 154(d)(4).	
7.	\boxtimes	Amendments to the claims of	he International Application under PCT Arti	cle 19 (35 U.S.C. 371 (c)(3))
		a. are attached hereto (r	equired only if not communicated by the Inte	ernational Bureau).
		b. \square have been communic	ated by the International Bureau.	
		c. \square have not been made;	however, the time limit for making such ame	endments has NOT expired.
		d. 🛮 have not been made a	and will not be made.	
8.		An English language translation	on of the amendments to the claims under PC	T Article 19 (35 U.S.C. 371(c)(3)).
9.	\boxtimes	An oath or declaration of the i	nventor(s) (35 U.S.C. 371 (c)(4)).	
10.	\boxtimes	An English language translation Article 36 (35 U.S.C. 371 (c)(on of the annexes of the International Prelimi 5)).	nary Examination Report under PCT
11.		A copy of the International Pr	eliminary Examination Report (PCT/IPEA/4	09).
12.	×	A copy of the International Se	arch Report (PCT/ISA/210).	
	_		ent(s) or information included:	
13.			ratement under 37 CFR 1.97 and 1.98.	A OF OTD 200 1001 111
14.		=	recording. A separate cover sheet in complia	ince with 37 CFR 3.28 and 3.31 is included.
15.	×	A FIRST preliminary amends		
16.		A SECOND or SUBSEQUE	NI preliminary amendment.	
17.		A substitute specification.	v and/or address latter	
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(703) 413-3000

Surinder Sachar

Registration No. 34,423

INTERNATIONAL APPLICATION NO. PCT/EP99/07899

U.S. APPLICATION NO. (IF KNOWN, SEE 37 CER

The following fees are submitted:.

BASIC NATIONAL FEE (37 CFR 1.492 (a) (1) - (5)) :

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	April	23	2001	
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ATTORNEY'S DOCKET NUMBER

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Amount to be: refunded

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IN THE UNITED STATES PATENT & TRADEMARK OFFICE

IN RE APPLICATION OF: :

BERND WENDEROTH ET AL : ATTN: APPLICATION DIVISION

SERIAL NO: NEW US PCT APPLN

(BASED ON PCT/EP99/07899)

FILED: HEREWITH :

FOR: PARAFFIN DISPERSANTS HAVING

A LUBRICITY EFFECT FOR

MINERAL OIL MIDDLE DISTILLATES

PRELIMINARY AMENDMENT

ASSISTANT COMMISSIONER FOR PATENTS WASHINGTON, D.C. 20231

SIR:

Prior to examination on the merits, please amend the above-identified application as follows.

IN THE CLAIMS

Please cancel Claims 3-11 and add the following claims:

- 12. (New) A mixture as claimed in claim 1, wherein the reaction product (a) is an amide, amidoammonium salt or ammonium salt in which no carboxyl group, one carboxyl group or a plurality of carboxyl groups is or are converted into amido groups.
- 13. (New) A mixture as claimed in claim 1, wherein the secondary amine of the component (a) is of the formula HNR₂, where R is straight-chain or branched C_{10-30} -alkyl.

- 14. (New) A mixture as claimed in claim 1, wherein the primary alkylamine of the component (b) is a C_{8-30} -alkylamine.
 - 15. (New) A mineral oil middle distillate containing a mixture as claimed in claim 1.
- 16. (New) A mineral oil middle distillate as claimed in claim 15, further comprising flow improvers, conductivity improvers, corrosion-inhibiting additives, lubricity additives, antioxidants, metal deactivators, antifoams, demulsifiers, detergents, cetane number improvers, dyes, fragrances or mixtures thereof.
- 17. (New) A concentrate containing 10-60% by weight, based on the total amount of the concentrate, of a mixture as claimed in claim 1, dissolved in the hydrocarbon solvent.
- 18. (New) A mineral oil middle distillate as claimed in claim 15, further comprising flow improvers based on ethylene/vinyl carboxylate copolymers.

REMARKS

Claims 1, 2 and 12-20 are active in the present application. Support for Claims 12-20 is found in Claims 3-11 and the specification. No new matter is added. An action on the merits and allowance of the claims is solicited.

Respectfully submitted,

OBLON, SPIVAK, McCLELLAND, MAIER & NEUSTADT, P.C.

Norman F. Oblon Attorney of Record Registration No. 24,618

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205736US0PCT

Marked-Up Copy	
Serial No:Amendment Filed on:	

IN THE CLAIMS

Claims 3-11 (Canceled.

- 12. (New)
- 13. (New)
- 14. (New)
- 15. (New)
- 16. (New)
- 17. (New)
- 18. (New)

O.Z. 0050/49464

"as originally filed"

Paraffin dispersants having a lubricity effect for mineral oil middle distillates

5 The present invention relates to mixtures suitable as paraffin dispersants having a lubricity effect, their use in mineral oil middle distillates, mineral oil middle distillates of this type and concentrates for this purpose.

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distillates. Mineral oil in particular distillates, such as gas oils, diesel oils or light fuel oils, which are obtained by distillation from mineral oils, have different paraffin depending on the origin of the crude oil. At relatively low temperatures, solid paraffins separate out (cloud point, CP). On further cooling, the lamellar n-paraffin crystals form a type of "house of cards structure" and the middle distillate sets although the predominant part of the middle distillate is still liquid. flowability of the middle distillate considerably impaired by the precipitated n-paraffins in the temperature range between cloud point and pour point; the paraffins block filters and result in a nonuniform supply of fuel to the combustion units or completely stop said supply. Similar faults occur in the case of light fuel oils.

It has long been known that the crystal growth of the n-paraffins in the combustion or power fuels obtained from mineral oil distillates can be modified by suitable additives. Effective additives prevent middle distillates from becoming solid at temperatures of only a few degrees Celsius below the temperature at which

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the first paraffin crystals separate out. Instead, well crystallized, separate paraffin crystals form, which crystals pass through filters in motor vehicles and heating systems or at least form a filter cake which is permeable for the liquid part of the middle distillates, so that trouble-free operation is ensured. According to European standard EN 116, the efficiency ofthe flow improvers is expressed indirectly by measuring the cold filter plugging point (CFPP).

Ethylene/vinyl carboxylate copolymers have long been used as flow improvers. The disadvantage of these additives is that, owing to their higher density compared with the liquid part, the precipitated paraffin crystals tend to settle out to an increasing extent on the bottom of the container on storage. Consequently, a homogeneous low-paraffin phase forms in upper part of the container and a two-phase paraffin-rich layer at the bottom. Since the middle distillate is generally taken off slightly above the bottom of the tank, both in the vehicle tanks and in storage or delivery tanks of the mineral oil dealers, there is a danger that the high concentration of solid paraffins will block filters and metering means. This danger is all the greater the greater the amount by the storage temperature is below precipitation temperature of the paraffins, since the precipitated paraffin increases with decreasing temperature.

These problems can be reduced by the additional use of paraffin dispersants (wax antisettling additives).

35 Thus, EP-A-0 398 101 describes reaction products of aminoalkylene polycarboxylic acids with long-chain, secondary amines as paraffin dispersants for mineral oil middle distillates. However, the effect is not sufficient in all mineral oil middle distillate

compositions, particularly when they have a low sulfur content of less than 500 ppm.

DE-A-11 49 843 describes the use of maleamic acids and their amine salts obtained from primary amines and maleic anhydride as corrosion inhibitors and stability improvers for mineral oil distillates as well as for preventing sediment formation. EP-A-0 106 234 describes the use of amine salts of maleamic acids obtained from primary amines and maleic anhydride as corrosion inhibitors for the storage and the transport of crude oils.

Since October 1996, only low-sulfur middle distillates having a sulfur content of not more than 500 ppm may be used as diesel fuels in the European Union, which fuels, owing to said sulfur content, help to achieve exhaust gases having a lower pollutant content. From the year 2000 onward, the maximum permissible sulfur content of diesel fuels in the European Union may not exceed 350 ppm. However, such diesel fuels have a substantially reduced lubricity, which can in some cases lead to high mechanical wear in distributor injection pumps of diesel engines.

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The lubricity of low-sulfur diesel fuels can be improved by adding lubricity additives. According to standard CEC F-06-A-96, the efficiency is determined by the HFRR test (High Frequency Reciprocating Rig test) by determining the wear size WS1.4 in μ m at 60°C; the smaller the WS1.4, the lower is the wear and the better is the lubricity.

There are numerous patent applications for products which can improve the lubricity of low-sulfur diesel fuels. WO 95/33805 states that flow improvers and paraffin dispersants, including reaction products according to EP-A-0 398 101, can improve the lubricity of middle distillates. However, the lubricity effect is

not sufficient in many mineral oil middle distillate compositions.

It is an object of the present invention to provide 5 improved products which ensure improved flowability of mineral oil middle distillates at low temperature by virtue of the fact that they have a dispersing effect such that settling of precipitated paraffins is delayed or prevented, and which simultaneously contribute to 10 improved lubricity of the mineral oil middle distillates.

We have found that this object is achieved, according to the invention, by a mixture containing

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(a) from 5 to 95% by weight of at least one reaction product of a poly(C_{2-20} -carboxylic acid) having at least one tertiary amino group with secondary amines and

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- (b) 5-95% by weight of at least one reaction product of maleic anhydride and a primary alkylamine.
- 25 The present invention also relates to the use of these additives for mineral oil distillates, in particular as paraffin dispersants and lubricity additives. The invention likewise relates to concentrates mineral oil middle and distillates 30 containing these mixtures.

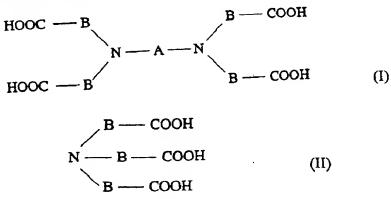
COMPONENT (a)

Component (a) is a reaction product of a poly(C_{2-20} -35 carboxylic acid) having at least one tertiary amino group with secondary amines.

The polycarboxylic acid preferably contains at least 3, particularly preferably 3 to 12, in particular 3 to 5,

carboxyl groups. The carboxyl groups in the polycarboxylic acid preferably have 2 to 10 carbon atoms, acetyl groups being preferred. The carboxyl groups are linked in a suitable manner to the polycarboxylic acid, for example via one or more C and/or N atoms. They are preferably bonded to tertiary nitrogen atoms which, in the case of a plurality of nitrogen atoms, are linked via hydrocarbon chains.

10 Component (a) is preferably an amide, amidoammonium salt or ammonium salt, or a mixture thereof, of aminoalkanecarboxylic acids of the formulae I and II



where A is straight-chain or branched alkylene of 2 to 6, preferably 2 to 4, in particular 2 or 3, carbon atoms, or a radical of the formula (III)

- where B is a radical of 1 to 19 carbon atoms, preferably a C_{1-19} -alkylene radical, particularly preferably C_{1-10} -alkylene, in particular a methylene radical. A is preferably an ethylene radical.
- 25 The secondary amine may be selected from a multiplicity of amines which carry hydrocarbon radicals which may be bonded to one another.

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The secondary amine is preferably of the formula HNR₂, where radicals R independently are straight-chain aliphatic radicals, in particular alkyl of 10 to 30, preferably 14 to 24, carbon atoms. They preferably have no hetero atoms or double or triple bonds. Preferably, the radicals R are identical.

The secondary amines can be bonded by means of amide structures or in the form of their ammonium salts to the polycarboxylic acid, also partly by means of amide structures and partly in the form of the ammonium salts. Preferably, little or no free acid groups are present.

15 Preferably, the amines are bonded completely in the form of the amide structures.

The amides or amidoammonium salts or ammonium salts of, for example, nitrilotriacetic acid, ethylenediamine-tetraacetic acid or 1,2-propylenediaminetetraacetic acid, are obtained by reacting the acids with from 0.5 to 1.5, preferably from 0.8 to 1.2, mol of amine per carboxyl group.

- The reaction temperatures are from about 80 to 200°C, the resulting water of reaction being continuously removed for the preparation of the amides. However, the reaction need not be continued completely to the amide; rather, from 0 to 100 mol% of the amine used may be present in the form of the ammonium salt. Particulary preferred amines are dioleylamine, dipalmitylamine, dicoconut fatty amine and dibehenylamine, in particular di-tallow fatty amine.
- 35 The novel components (a) of the mixture and their preparation are described in EP-A-0 398 101. The reaction product of one mole of ethylenediaminetetra-acetic acid and four moles of hydrogenated di-tallow fatty amine is particularly preferred.

If required, small amounts of conductivity improvers in the form of salts, in particular of hydrocarbon-soluble carboxylic acids and sulfonic acids or their metal and ammonium salts, may also be added to the components (a) of the mixture.

Component (b)

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Preparation of the novel components (b) of the mixture 10 is carried out in a manner known per se by reacting anhydride with C_{8-30} -alkylamines, preferably primary C_8-C_{18} -alkylamines, in a molar ratio of 1:1 at by the process described 70 to 100°C DE-A-11 49 843 and EP-A-0 106 234; suitable primary 15 amines are all amines defined within these limits, for example straight-chain or branched octyl-, decyl-, undecyl-, dodecyl-, tridecyl-, tetradecyl-, pentadecyl-, hexadecyl-, heptadecyl- and octadecylamine 20 and mixtures of these amines. The reaction product of one mole of maleic anhydride and one mole of tridecylamine is particularly preferred.

The novel mixtures can be prepared by simple mixing of the components (a) and (b); these mixtures are added to the mineral oil distillates in amounts of 10-1000 ppm, preferably from 50 to 500 ppm. The amount of the component (a) is from 5 to 95, preferably from 30 to 95, in particular from 50 to 90, % by weight and the amount of the component (b) is from 5 to 95, preferably from 5 to 70, in particular from 10 to 50, % by weight.

The novel polymer mixtures are used as additives for mineral oil middle distillates, which are understood as meaning petroleum, light fuel oils and diesel fuels having a boiling point of from about 150 to 400°C. The polymer mixtures may be added to the middle distillates directly but are preferably added as a 20 to 70% by weight strength solution (concentrate). Suitable

solvents are aliphatic or aromatic solvents, such as xylene or mixtures thereof, and furthermore high-boiling aromatics mixtures, such as solvent naphtha, and middle distillates. The amount of mixture in the mineral oil middle distillates is as a rule from 10 to 10,000, preferably from 20 to 5000, particularly preferably from 50 to 1000, ppm.

As a rule, the middle distillates also contain flow for example based on ethylene/vinyl 10 improvers, carboxylate copolymers. Depending on the intended use, the middle distillates may additionally contain further conductivity additives. e.q. improvers, additives, lubricity additives. inhibiting oxidants, metal deactivators, antifoams, demulsifiers, 15 detergents, cetane number improvers and/or dyes and fragrances.

The novel mixtures result in a substantial improvement in the low-temperature flow properties in middle distillates, regardless of their origin, in that they effectively keep the paraffin crystals which separate out in suspension so that there is no blocking of filters and pipes by paraffin which has settled out.

They have a broad action and thus ensure that the paraffin crystals which have separated out are very well dispersed in various middle distillates; at the same time, they help to improve the lubricity of the middle distillates.

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The effect of the combination of the components (a) and (b) is substantially better than the effect of the individual components at the same dose.

35 The examples which follow illustrate the invention.

EXAMPLES:

Example 1 (component (a))

240 g (0.48 mol) of hydrogenated di-tallow fatty amine (Armeen® 2HT from Akzo) and 35 g (0.12 mol) of ethylenediaminetetraacetic acid were melted and were heated to 190°C, the resulting water of reaction being distilled off continuously. The reaction was terminated after about 25 hours at an acid number of less than 10 and an amine number of less than 1.1. By applying reduced pressure from a waterjet pump (2 hours, 120°C), the water of reaction was removed completely. 265 g of a light brown, waxy solid were obtained. The product obtained was diluted with solvent naphtha so that the solids content of the product was 50% by weight.

15 Example 2 (component (b))

A mixture of 98 g (1.0 mol) of maleic anhydride and 199 g (1.0 mol) of tridecylamine was heated in 250 ml of solvent naphtha at about 70°C for 2 hours while stirring. The light brown, clear solution obtained was then diluted with solvent naphtha so that the solids content of the product was 50% by weight.

Use Examples:

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The novel mixtures were tested in two commercial German winter diesel fuels which complied with European diesel fuel standard EN 590; they are designated as D1 and D2 and are characterized by the following physical data:

	D 1 (97/526)	D 2 (96/86)
Cloud point (°C) according to ISO 3015:	-6	-6
CFPP (°C) according to	-10	-8
EN 116: Density at 15°C (kg/m³) according to ASTM D 4052:	841	834
Sulfur content (ppm) according to EN 24260:	160	200
WS1.4 (μm) according to CEC F-06-A-96:	542	
Distillation according to		
ISO 3405: Initial boiling point (°C)	170	171
5% boiling point (°C)	203	193
10% boiling point (°C)	215	200
20% boiling point (°C)	235	212
50% boiling point (°C)	280	249
70% boiling point (°C)	308	282
90% boiling point (°C)	347	329
95% boiling point (°C)	364	345
Final boiling point (°C)	371	360

The following mineral oil middle distillate compositions were tested:

Mineral oil middle distillate compositions containing

as paraffin dispersant

one of the novel mixtures PD 1 (consisting of 83% by weight of component (a) from Example 1 and 17% by weight of component (b) from Example 2), PD 2 (consisting of 50% by weight of component (a) from Example 1 and 50% by weight of component (b) from Example 2), PD 3 (consisting of 67% by weight of component (a) from Example 1 and 33% by weight of

component (b) from Example 2) or PD 4 (consisting of 90% by weight of component (a) from Example 1 and 10% by weight of component (b) from Example 2) and, as comparative examples, the respective individual components from Example 1 and Example 2 or none of the components (Comparative Examples V2, V3, V1). V1 thus contains only MDFI as additive

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2. as flow improver MDFI

a product based on ethylene/vinyl carboxylate which is marketed under the tradename Keroflux $^{\otimes}$ ES 6100 by BASF AG.

Description of the test method:

The middle distillates were mixed with the amounts, stated in the table, of the novel mixtures PD 1 to PD 4 or of Examples 1 and 2 and of the flow improver MDFI at 40°C while stirring and then cooled to room temperature.

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For the additive-containing middle distillate samples, the cold filter plugging point (CFPP) according to EN 116 was determined, and in some cases also the WS1.4 according to CEC-F-06-A-96.

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The additive-containing middle distillates were cooled in 500 ml glass cylinders in a refrigerant bath from room temperature to -13°C at a cooling rate of about 14°C per hour and were stored at this temperature for 20 hours. The amount and appearance of the paraffin phase were then determined and assessed visually.

The cold filter plugging point (CFPP) according to EN 116 and the cloud point (CP) according to ISO 3015

were determined for the 20% by volume bottom phase separated off at -13° C from each sample. The smaller the deviation of the cloud point of the 20% by volume bottom phase from the original CP of the respective middle distillate, the better are the paraffins dispersed.

The results obtained are shown in Tables 1 and 2:

10 Table 1: Dispersing experiments in D 1, CP: -6° C, CFPP: -10° C, WS1.4: 542 μm

Mix- ture	Dose	MDFI	WS1.4	CFPP	Paraf- fin	Dis- persed	20% be	ottom
	(ppm)	(ppm)	(µm)	(°C)	sedi- ment (% by vol- ume)	<pre>paraf- fins (% by vol ume)</pre>	CFPP (°C)	CP (°C)
PD 1	150	200		-30	10	90	-29	-6
PD 2	150	200	310	-25	10	90	-27	-6
PD 3	150	200	-	-26	10	90	-28	-6
PD 4	150	200	328	-28	10	90	-27	-5
V1		200	526	-25	44	0	-18	0
V2	150	200	394	-25	46	54	-20	-2
V3	150	200	369	-23	42	58	-23	-3

Table 2: Dispersing experiments in D 2, CP: -6° C, 15 CFPP: -8° C

Mix- ture	Dose	MDFI	CFPP	Paraffin sediment	Dispersed paraffins	20% bo	ttom
	(ppm)	(ppm)	(°C)	(% by volume)	(% by volume)	CFPP (°C)	CP (°C)
PD 1	300	300	-23	6	94	-18	-5
PD 3	300	300	-20	8	92	-27	~5
PD 4	300	300	-29	8	92	-20	-5
V1		300	-22	30	О	1	+3
V2	300	300	-30	10	90	-20	-3
v3	300	300	-20	30	70	-7	+2

The test results show that, in the mineral oil middle distillates, the novel mixtures result in a lower cloud point of the 20% bottom phase than the mixtures of the comparative examples.

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This shows that, in mineral oil middle distillates, regardless of their origin, the precipitated paraffin crystals are effectively kept in suspension by the novel mixtures of the components (a) and (b) so that filters and pipes are not blocked by paraffin which settles out. The novel mixtures have a very broad action and ensure that the paraffin crystals which separate out are very well dispersed in various middle distillates.

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At the same time, the tests results show that, at the same total dose, the novel mixtures lead to a lower WS1.4 and hence to improved lubricity of low-sulfur diesel fuels then the respective individual components.

Claims as enclosed to IPER

We claim: 5

A mixture containing 1.

- (a) from 5 to 95% by weight of at least one reaction product of a poly(C2-20-carboxylic 10 acid) having at least one tertiary amino group with secondary amines and
- (b) 5-95% by weight of at least one reaction product of maleic anhydride and a primary 15 alkylamine.
- A mixture as claimed in claim 1, wherein the 2. $poly(C_{2-20}-carboxylic acid)$ having at least one tertiary amino group is of the following formula I 20 or II

HOOC — B
$$N - A - N$$
 $B - COOH$

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where A is a straight-chain or branched C2-6alkylene radical or a radical of the formula III

$$--CH2 ---CH2 --$$

where B is a C_{1-19} -alkylene radical.

- 3. A mixture as claimed in claim 1 or 2, wherein the reaction product (a) is an amide, amidoammonium salt or ammonium salt in which no carboxyl group, one carboxyl group or a plurality of carboxyl groups is or are converted into amido groups.
- 4. A mixture as claimed in any of claims 1 to 3, wherein the secondary amine of the component (a) is of the formula HNR_2 , where R is straight-chain or branched C_{10-30} -alkyl.
- 5. A mixture as claimed in any of claims 1 to 4, wherein the primary alkylamine of the component (b) is a C_{8-30} -alkylamine.
- 6. The use of a mixture as claimed in any of claims 1 to 5 as an additive for mineral oil middle distillates.
 - 7. The use as claimed in claim 6 as a paraffin dispersant and lubricity additive for mineral oil middle distillates.

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- 8. A mineral oil middle distillate containing a mixture as claimed in any of claims 1 to 5.
- A mineral oil middle distillate as claimed in 9. 30 claim 8, furthermore containing flow improvers, improvers, conductivity corrosion-inhibiting additives, lubricity additives, antioxidants, metal deactivators, antifoams, demulsifiers, detergents, cetane number improvers, 35 fragrances or mixtures thereof.
 - 10. A concentrate containing 10-60% by weight, based on the total amount of the concentrate, of a

mixture as claimed in any of claims 1 to 5, dissolved in the hydrocarbon solvent.

11. A mineral oil middle distillate as claimed in claim 8, further containing flow improvers based on ethylene/vinyl carboxylate copolymers.

Abstract

The mixture contains

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(a) from 5 to 95% by weight of at least one reaction product of a $poly(C_{2-20}-carboxylic$ acid) having at least one tertiary amino group with secondary amines and

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(b) from 5 to 95% by weight of at least one reaction product of maleic anhydride and a primary alkylamine.

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Declaration, Power of Attorney

Page 1 of 3

0050/049464

We (I), the undersigned inventor(s), hereby declare(s) that:

My residence, post office address and citizenship are as stated below next to my name,

We (I) believe that we are (I am) the original, first, and joint (sole) inventor(s) of the subject matter which is claimed and for which a patent is sought on the invention entitled

Paraffin dispersants having a lubrictiy effect for mineral oil middle distillates

the specification of which	
[] is attached hereto.	
[] was filed on	as
Application Serial No.	
and amended on	
[x] was filed as PCT international application	
NumberPCT/EP99/07899	
on19/10/1999	
and was amended under PCT Article 19	
on (if applicab	le)

- We (I) hereby state that we (I) have reviewed and understand the contents of the above—identified specification, including the claims, as amended by any amendment referred to above.
- We (I) acknowledge the duty to disclose information known to be material to the patentability of this application as defined in Section 1.56 of Title 37 Code of Federal Regulations.
- We (I) hereby claim foreign priority benefits under 35 U.S.C. § 119(a)—(d) or § 365(b) of any foreign application(s) for patent or inventor's certificate, or § 365(a) of any PCT International application which designated at least one country other than the United States, listed below and have also identified below, by checking the box, any foreign application for patent or inventor's certificate, or PCT International application having a filing date before that of the application on which priority is claimed. Prior Foreign Application(s)

Application No.	Country	Day/Month/Year	Priority Claimed	:001 - 55
19848621.9	Germany	21 October 1998	[x] Yes [] No	odosopa

) hereby claim the benefit under Title 35, on(s) listed below.	United States Codes, § 119(e) of any United States provis	ional
(Application Number)	(Filing Date)	
(Application Number)	(Filing Date)	

We (I) hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s), or § 365(c) of any PCT International application designating the United States, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT International application in the manner provided by the first paragraph of 35 U.S.C. § 112, I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR § 1.56 which became available between the filing date of the prior application and the national or PCT International filing date of this application.

Application Serial No.	Filing Date	Status (pending, patented, abandoned)

And we (I) hereby appoint: Norman F. Oblon, Reg. No. 24,618; Marvin J. Spivak, Reg. No. 24,913; C. Irvin McClelland, Reg. No. 21,124; Gregory J. Maier, Reg. No. 25,599; Arthur I. Neustadt, Reg. No. 24,854; Richard D. Kelly, Reg. No. 27,757; James D. Hamilton, Reg. No. 28,421; Eckhard H. Kuesters, Reg. No. 28,870; Robert T. Pous, Reg. No. 29,099; Charles L. Gholz, Reg. No. 26,395; William E. Beaumont, Reg. No. 30,996; Jean-Paul Lavalleye, Reg. No. 31,451; Stephen G. Baxter, Reg. No. 32,884; Richard L. Treanor, Reg. No. 36,379; Steven P. Weihrouch, Reg. No. 32,829; John T. Goolkasian, Reg. No. 26,142; Richard L. Chinn, Reg. No.34,305; Steven E. Lipman, Reg. No 30,011; Carl E. Schlier, Reg. No. 34,426; James J. Kulbaski, Reg. No. 34,648; Richard A. Neifeld, Reg. No. 35,299; J. Derek Mason, Reg. No. 35,270; Surinder Sachar, Reg. No. 34,423; Christina M. Gadiano, Reg. No. 37,628; Jeffrey B. McIntyre, Reg. No. 36,867; William T. Enos, Reg. No. 33,128; Michael E. McCabe, Jr., Reg. No. 37,182; Bradley D. Lytle, Reg. No. 40,073; and Michael R. Casey, Reg. No. 40,294; our (my) attorneys, with full powers of substitution and revocation, to prosecute this application and to transact all business in the Patent Office connected therewith; and we (I) hereby request that all correspondence regarding this application be sent to the firm of OBLON, SPIVAK, McCLELLAND, MAIER & NEUSTADT, P. C., whose Post Office Address is: Fourth Floor, 1755 Jefferson Davis Highway, Arlington, Virginia 22202.

CHOHOMORNE ZUYER

We (I) declare that all statements made herein of our (my) own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issuing thereon.

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